

**Amendments to the Claims:**

This list of claims will replace all prior version, and listings, of claims in the application.

**Listing of Claims:**

1-14. (cancelled).

15. (new) A process for recovery of common salt and marine chemicals from brine in an integrated manner, said process comprising the sequential steps of:

(i) treating brine with a composition comprising calcium chloride to produce a calcium sulphate precipitate;

(ii) separating the precipitated calcium sulphate from the brine to obtain partly desulphated brine;

(iii) treating the partly desulphated brine obtained in step (ii) with barium chloride to obtain substantially desulphated brine;

(iv) evaporating the substantially desulphated brine thus obtained in step (iii) to a density of 29-32° Be' to obtain crystals of common salt having a negligible amount of sulphate salts, and a bittern;

(v) washing the common salt thus obtained in step (iv) with water or dilute brine to remove adhering chlorides of calcium and magnesium;

(vi) evaporating the bittern obtained in step (iv) up to a density of about 35.5° Be' to obtain crude carnallite and a concentrated end bittern comprising magnesium chloride and enriched bromide;

(vii) solidifying a part of the end bittern and calcining the solidified part to produce solid magnesium oxide and hydrochloric acid; and

(viii) reacting the hydrochloric acid produced in step (vii) with a calcerous material comprising limestone to provide calcium chloride, and recycling the calcium chloride to step (i).

16. (new) The process as claimed in claim 15, wherein the recovered marine chemicals include, potassium chloride, magnesium chloride enriched with bromide, high purity magnesia and calcium sulphate, each containing less than 0.5% chloride.

17. (new) The process as claimed in claim 15, wherein the brine treated in step (i) has a concentration in the range of 3 to 24 g/l.

18. (new) The process as claimed in claim 1, wherein the composition comprising calcium chloride in step (i) is pure calcium chloride or soda ash distiller waste.

19. (new) The process as claimed in claim 18, wherein the soda ash distiller waste contains 5-15% calcium chloride.

20. (new) The process as claimed in claim 18, wherein the pure calcium chloride is prepared by reacting hydrochloric acid with calcerous material.

21. (new) The process as claimed in claim 15 wherein in step (i), the calcium chloride has a concentration in the range of 100 to 600 g/L.

22. (new) The process as claimed in claim 15 wherein in step (ii), the precipitated calcium sulphate is separated in granular form from the brine by a seeding process.

23. (new) The process as claimed in claim 15 wherein in step (iii), 0.80-0.95 mole ratio of barium to residual sulphate ion in the form of  $\text{BaCl}_2$  is used.

24. (new) The process as claimed in claim 15 wherein in step (iv), evaporation of the bittern is carried out in solar pans.

25. (new) The process as claimed in claim 15 wherein in step (iv), the bittern is evaporated to a density of in the range from 29 to 35.5 °Be°.

26. (new) The process as claimed in claim 15 wherein in step (vi), the crude carnallite is obtained in the form of crystals.

27. (new) The process as claimed in claim 15 wherein in step (vi), the carnallite thus obtained has the composition 15.00% KCl; 28.22%  $\text{MgCl}_2$ ; 0.46%  $\text{CaSO}_4$ ; 0.36%  $\text{CaCl}_2$ ; and 6.2% NaCl.

28. (new) The process as claimed in claim 15 wherein in step (vi), the carnallite thus obtained is decomposed to obtain marine salts.

29. (new) The process as claimed in claim 28 wherein potassium chloride is recovered from the marine salts.

30. (new) The process as claimed in claim 15 wherein in step (vii), the solidified end bittern is calcined at 600 to 800°C to obtain MgO and HCl.

31. (new) The process as claimed in claim 15 wherein in step (vii), the HCl obtained upon calcinations of the end bittern in step (vii) is reacted with a calcerous material to prepare calcium chloride.

32. (new) The process as claimed in claim 15 wherein in step (i), the sulphate concentration of the brine is in the range of 5 to 18 g/L at 16°Be'.

33. (new) The process as claimed in claim 15 wherein in step (ii), the sulphate concentration of the brine is in the range of 0.5 to 2.0 g/L.

34. (new) The process as claimed in claim 15 wherein the brine treated in step (i) is sub-soil brine having up to 18°Be' of sodium chloride and less than 6 g/L of sulphate at 16°Be'.

35. (new) The process as claimed in claim 15, wherein the bromide concentration in the concentrated end bittern from step (vi) is up to 7.5 g/L at 35.5 °Be'.